

Understanding Corrosion Mechanisms in Oxy-Fired Systems

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oxidation experiments

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T. Lowe - SEM, image analysis

D. Leonard - EPMA

12MWh/yr per U.S. resident Where will it come from?

coal?
how?

Conventional: "USC"

-PC Turk, AR, 595°C

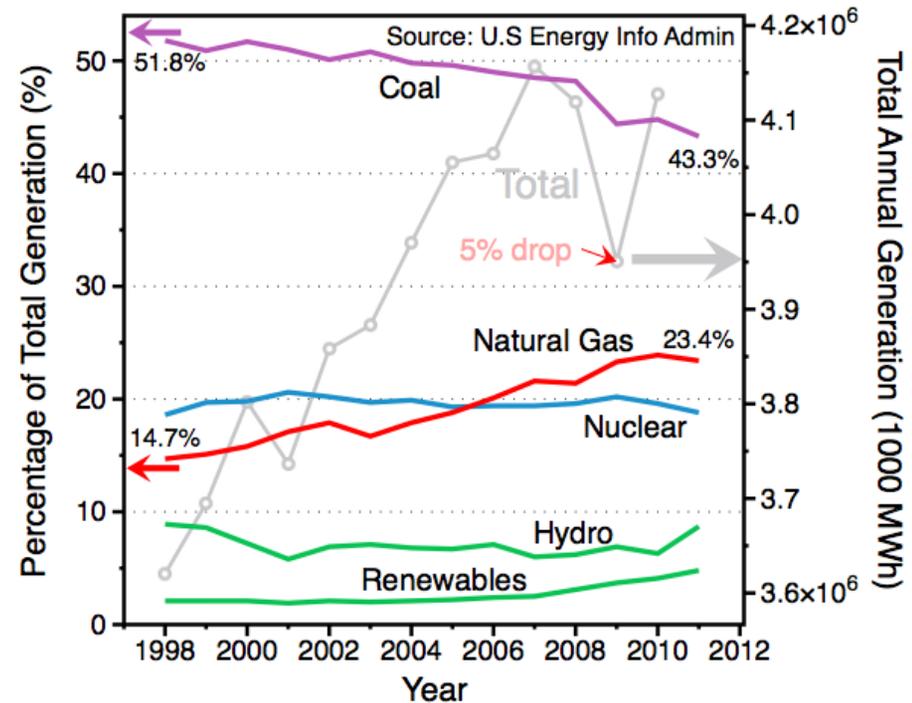
Gasification:

-IGCC Kemper Co., MS

-IGCC Edwardsport, IN

Oxy-firing:

-FutureGen 2.0 (?)

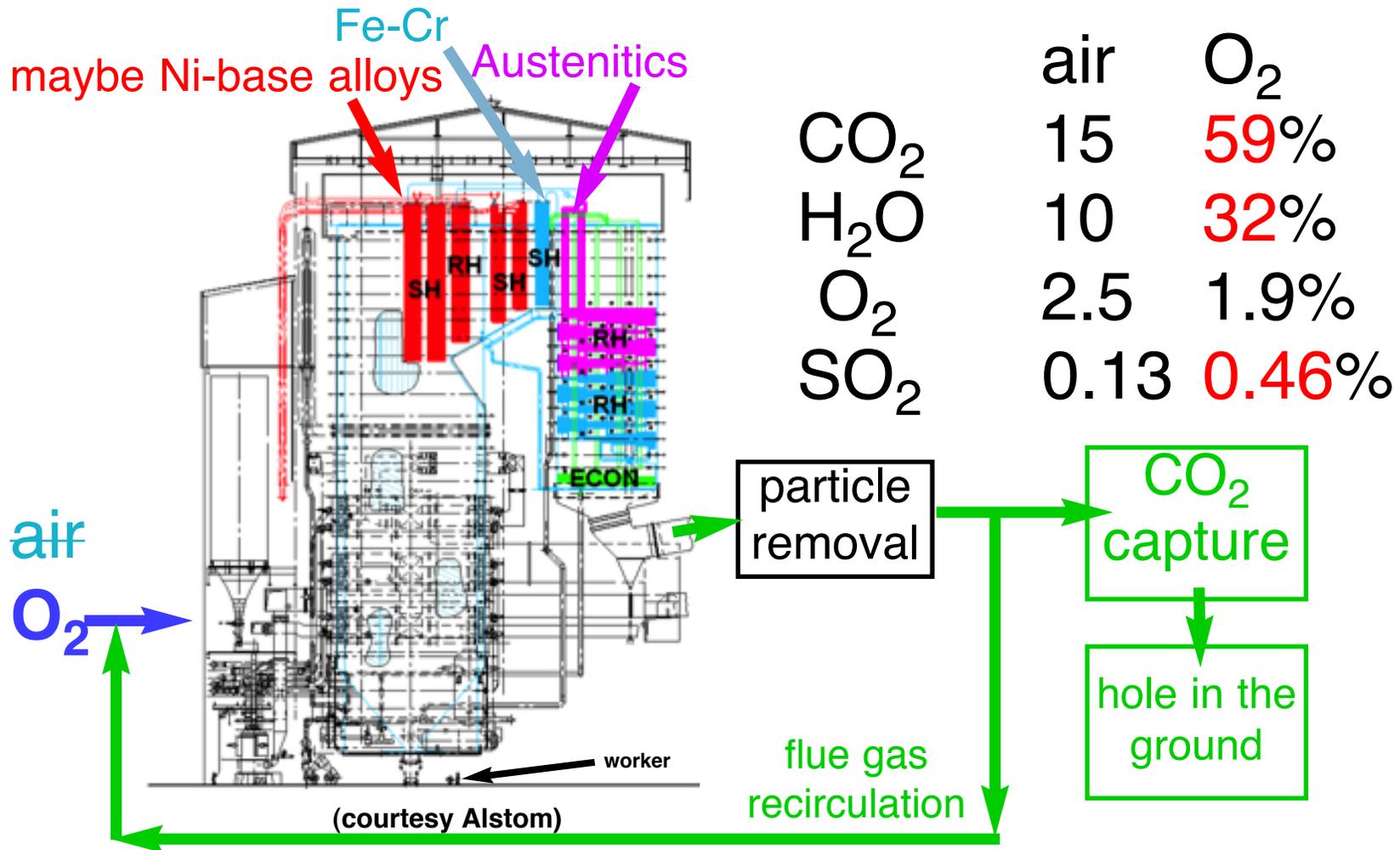


vs.



FutureGen 2.0: U.S. demo of oxy-firing

Germany: 30MW oxy-fired pilot plant (Alstom)



Several studies published by Alstom (Bordenet)
Oxy-firing literature tends to focus on worst case

Current Tasks & Timeline

Goal: Mechanistic understanding to enable accurate oxy-fired corrosion modeling

1. Steam/gas corrosion (no ash)
 2. Fireside corrosion (with ash)
 3. Environment-mechanical property effect
 - effect of steam on creep (Dryepondt)
 4. Coatings
 - fabrication and model (TTU subcontract)
 - effect on mechanical properties (Dryepondt)
- A. ~600°C ferritic/martensitic steels (FY10-12)
- B. ~650°-700°C austenitic steels (FY11-13)
- C. ~700°-750+°C Ni-base alloys
 - creep testing at 800°C (FY11-12)
 - ash testing 600°-800°C (FY12)

What's different here?

Many previous & current studies of oxy-firing & CO₂

- “Oxy” worse: Speigel (2006) + Corvino (2008)
- Complicated: boiler OEMs have advantage
- CO₂ effect: Jülich, U. Pitt & Australia (Young)

Issues with fireside corrosion experiments:

Different experimental conditions (if published)

1000h vs. 10 x 100h (ash re-supply)

Ash/gas/temp. variables

Use of Pt catalyst (SO₂/SO₃)

*** Evaluate experimental parameters (FY12)**

Typically, only commercial alloys evaluated

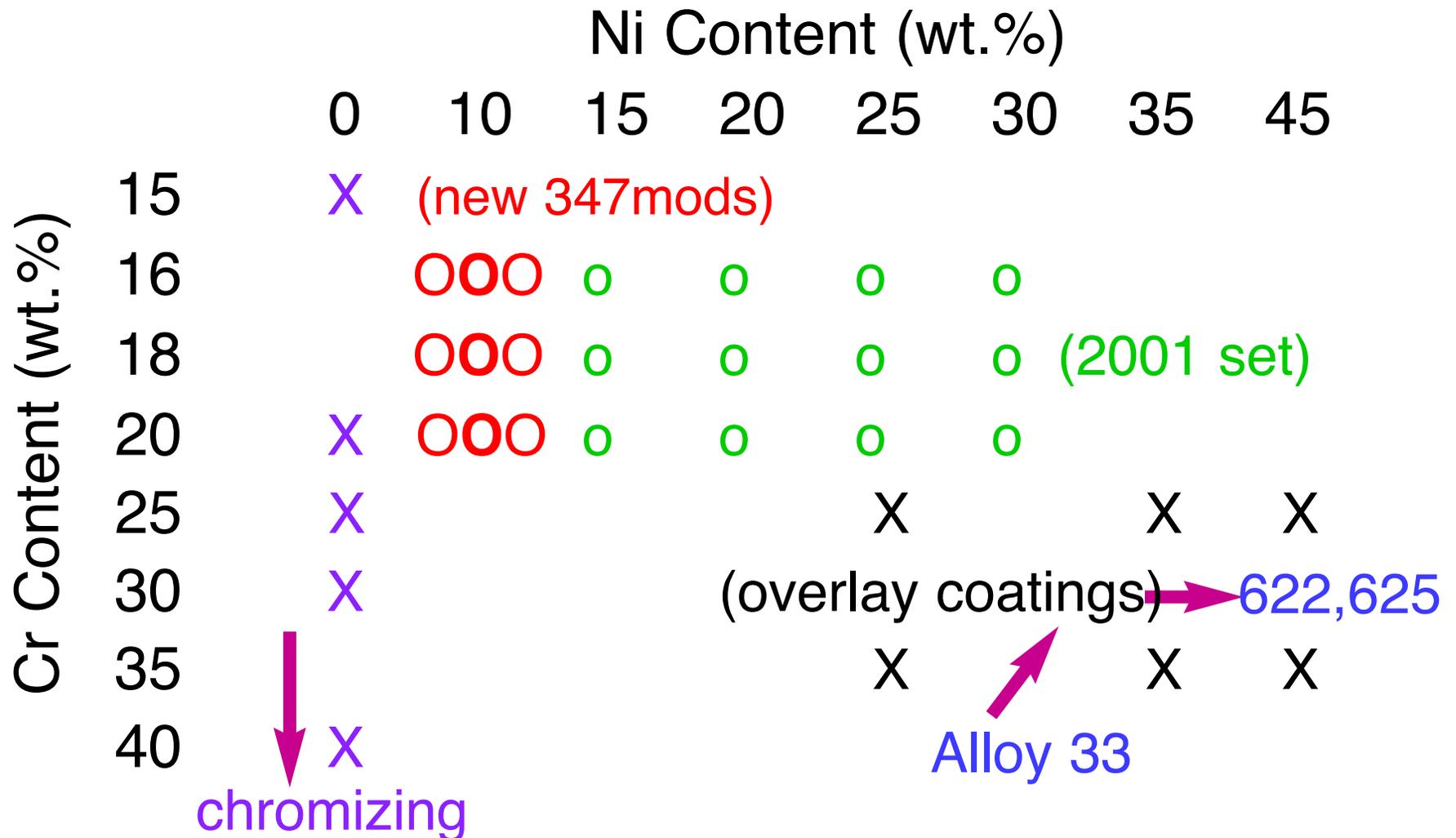
Prior work showing Cu-containing alloy attacked

Was it an effect of Cu or other element(s)?

*** Model alloys to better understand composition**

Not just commercial alloys

Model alloys: better composition understanding



Cast 400g, hot-roll to 8mm: cut coupons & rods

Corrosion testing w/o ash

Determine effect of higher CO₂, H₂O, SO₂...



17bar or 1bar

gas only, no ash

- H₂O only

- Ar-50%CO₂*

- H₂O-50%CO₂*

(*CO₂+1500ppmO₂)



Synthetic ash: 30%Fe₂O₃-30%Al₂O₃-

30%SiO₂-5%Na₂SO₄-5%K₂SO₄

Gas: N₂-CO₂-H₂O-O₂-SO₂

Temperature: 600°C

Time: 500h (1 cycle)



25x6mm rod in porous alumina

Continuing to establish methodology + procedure

- Current focus on characterization process

Summary: Gas only exposure

1. 600°C:

- a. steam 1 bar FY11, 2kh
- b. Ar-50%(CO₂-0.15O₂)(buffer) FY11, 2kh
- c. 50%(CO₂-0.15O₂)-50%H₂O FY11, 5kh
- d. 50%CO₂-50%H₂O(no buffer) FY12, 2kh
- e. Ar-10%(CO₂-0.15O₂)-50%H₂O FY12, 2kh
- f. Ar-50%H₂O started

2. 650°C:

- a. steam 1 bar FY11-12, 5kh
- b. 50%(CO₂-0.15O₂)-50%H₂O started
- c. Ar-50%(CO₂-0.15O₂) next

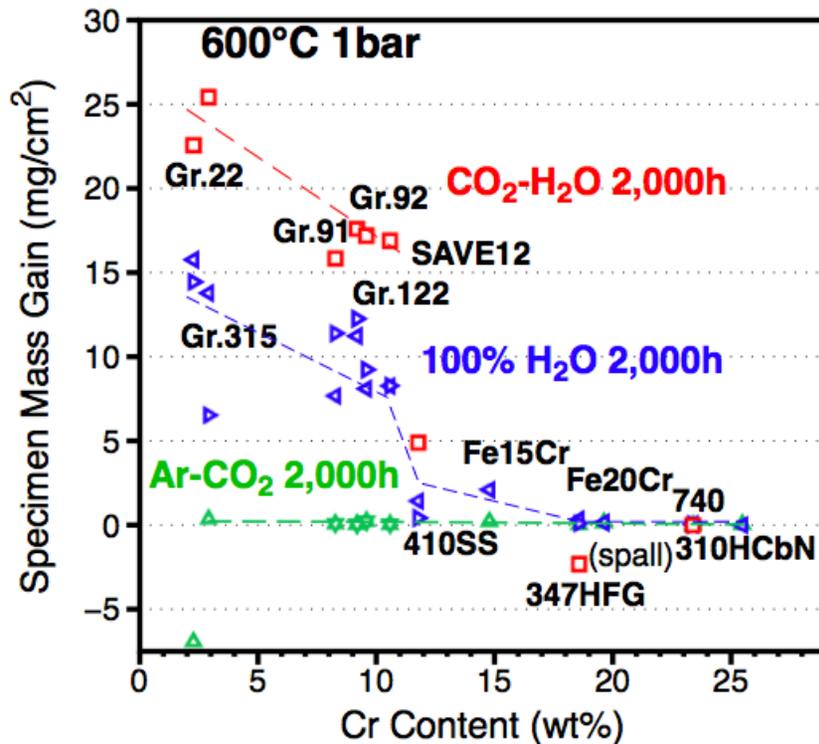
3. 800°C steam 17bar: A-USC follow on, started

4. 550°C steam 1bar (compare 17bar) started

600°C: CO₂ content and buffer

Followup on H₂O-50%(CO₂-0.15O₂)

FY11 results



Mass gain after 2,000h
Worst case (fastest rate):

O₂ buffered
50%H₂O-50%CO₂

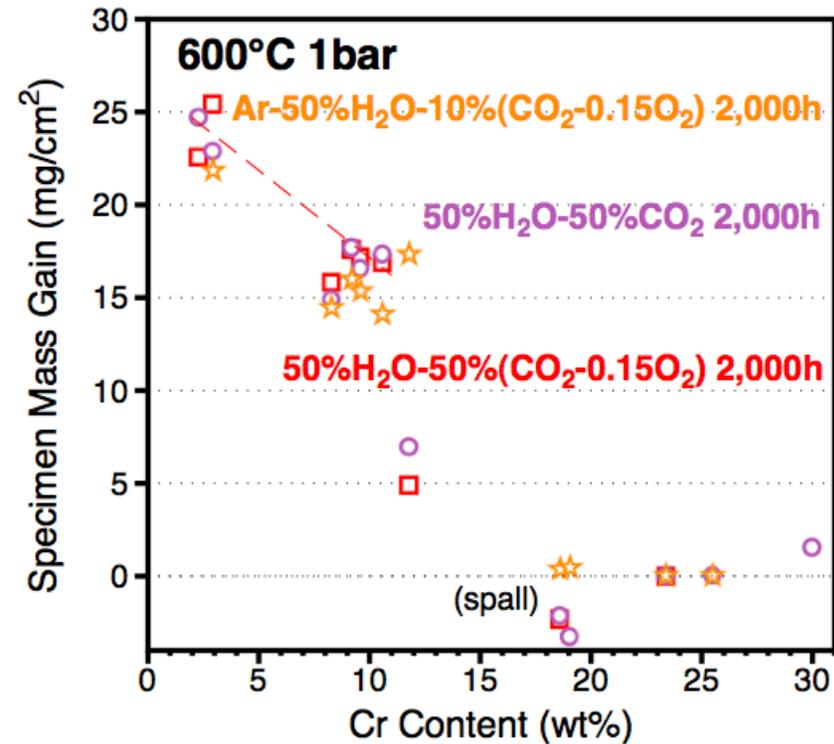
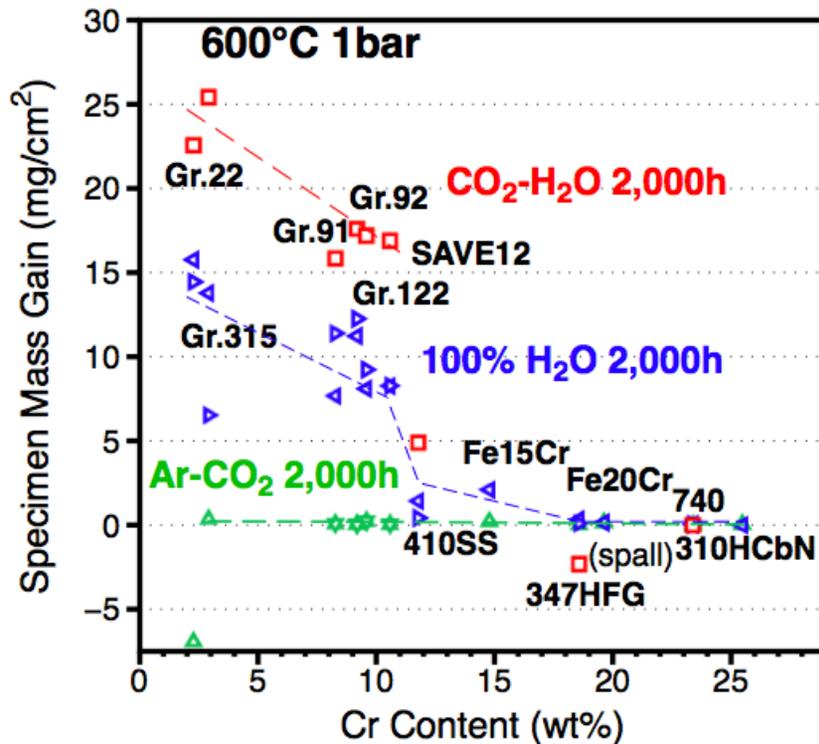
Most other groups do not use buffer, what is its role?

Little effect of C(CO₂) & buffer

600°C, 4 x 500h cycles, 1bar

FY11 results

FY12 results



No buffer: 50%H₂O-50%CO₂

Lower CO₂: Ar-50%H₂O-10%(CO₂-0.15O₂)

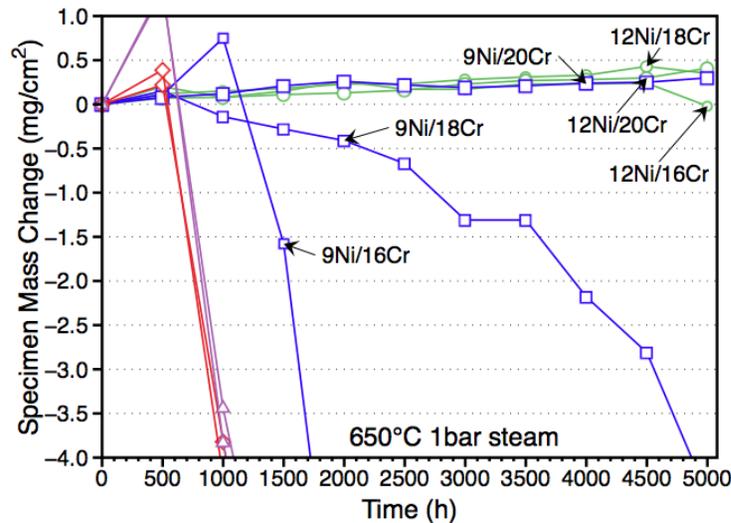
Both: little effect on 2,000h mass change

Need to complete metallography comparison

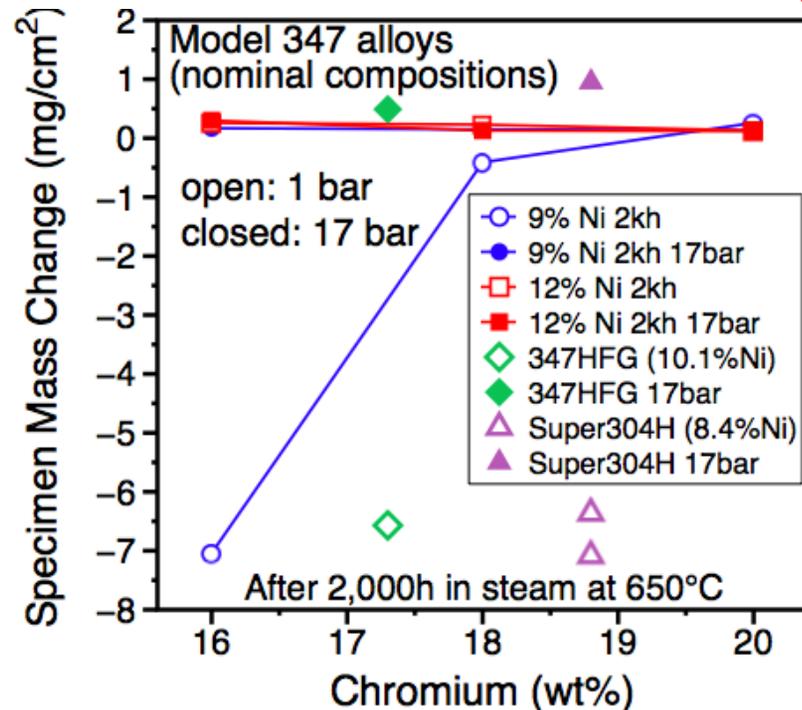
Model 347 alloys: 650°C steam

Cast, hot rolled Fe-Cr-Ni-1.5Mn-0.4Si-0.8Nb-0.09C

1 bar mass gain:



1 & 17bar 2,000h summary:



5,000h 1bar exposure completed in March 2012

Higher (12%) Ni content very beneficial

2000h 17bar completed April 2012 (no effect)

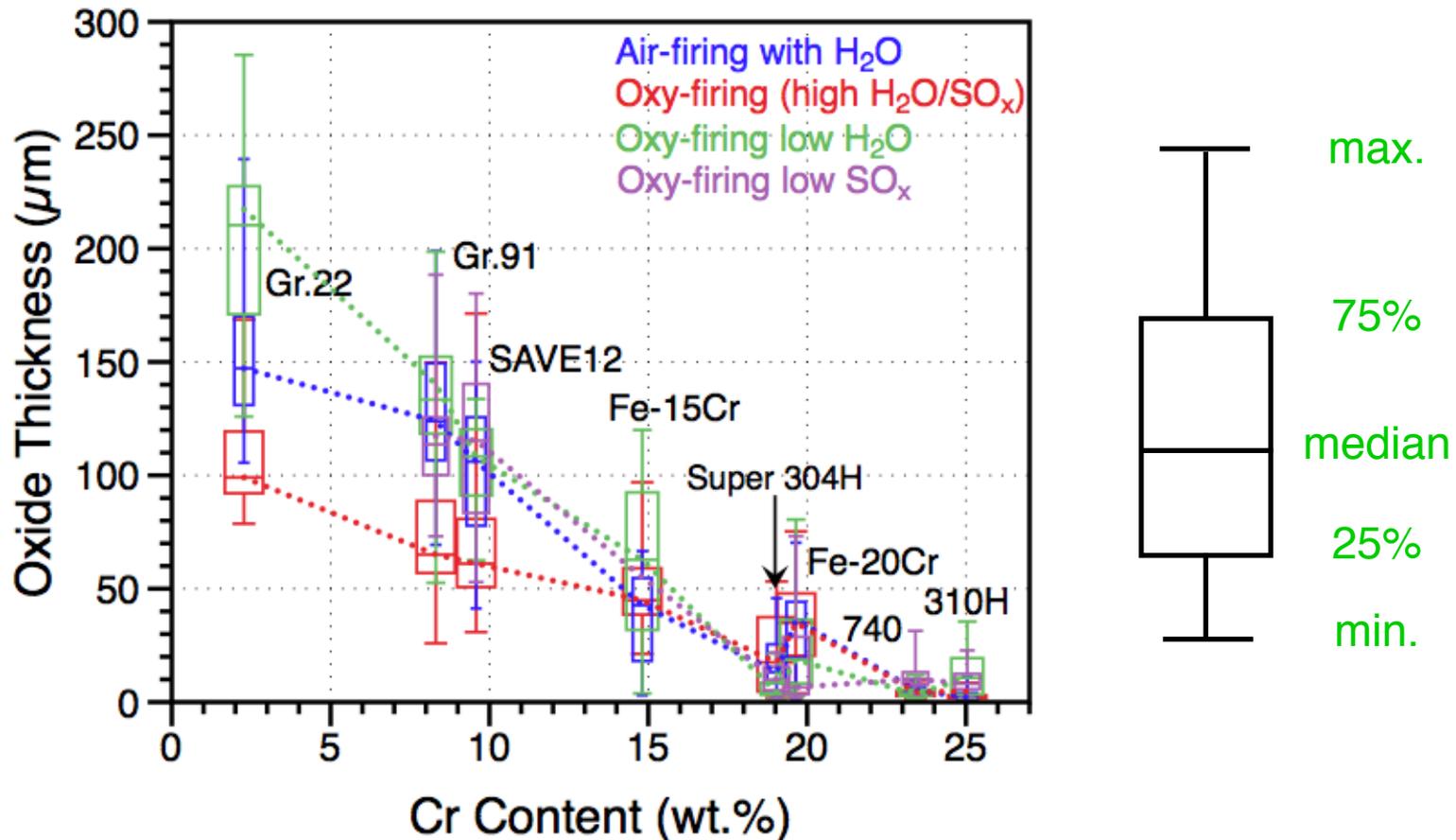
Concern: model alloys better than 347HFG & S304H

Summary: Ash exposure

1. 600°C: (oxy-fire retrofitting current plants)
air/oxy-firing (hot gas recirculation) (done)
low H₂O/low SO₂ (done)
FY12: low H₂O/low SO₂ (cold gas recirculation)
2. 650°C: (current USC plants)
air/oxy-firing (run/awaiting metallography)
3. 700°C:
air/oxy-firing (later this year)
4. 750°C: (A-USC range)
air/oxy-firing (run/awaiting metallography)
5. 800°C: (A-USC range)
air/oxy-firing (later this year)

Little effect of gas at 600°C

Synthetic coal ash, 500h exposures in 4 gases



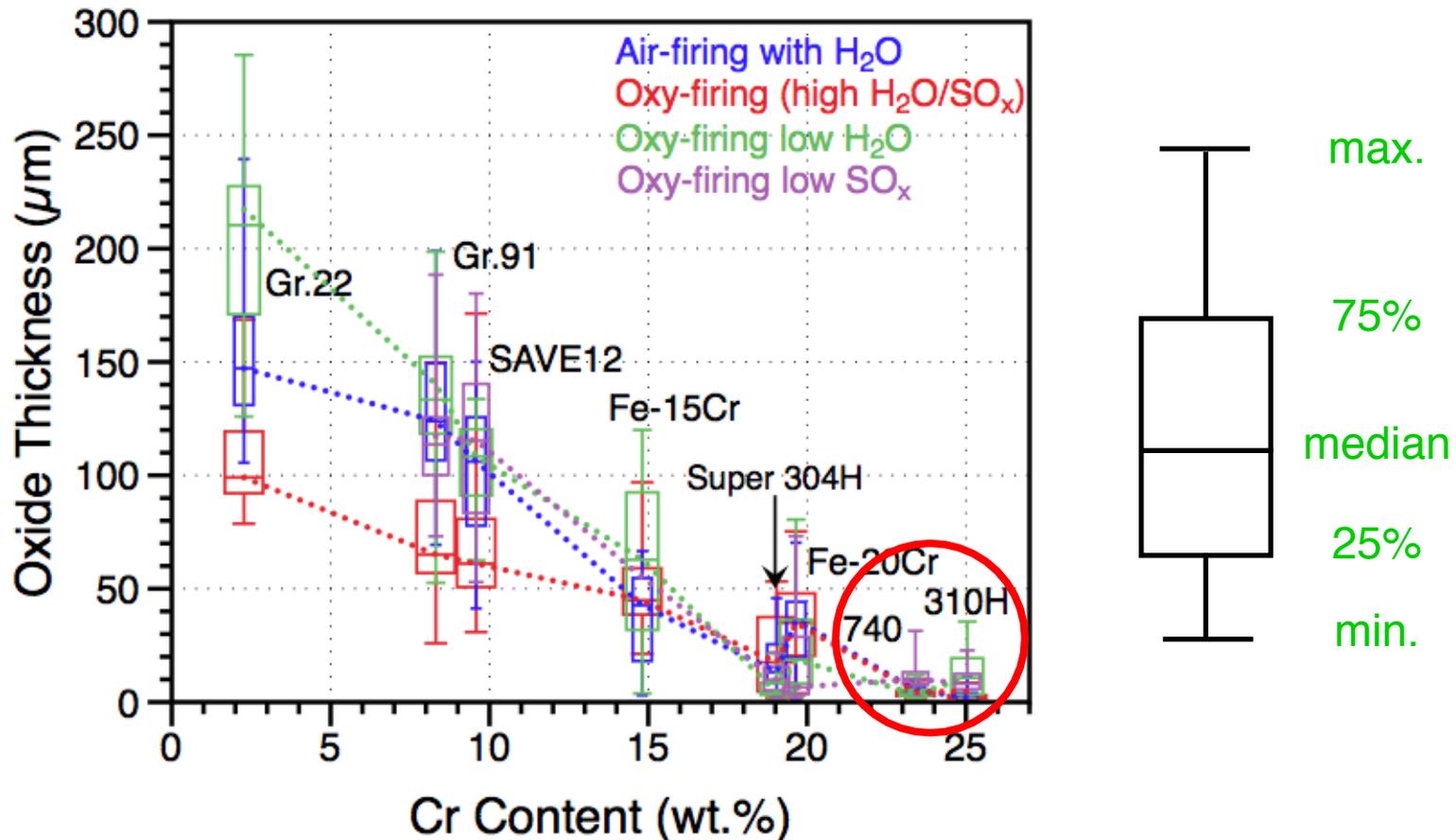
Higher CO₂ environments not detrimental

Expected the lower SO₂ environment to lower attack

- same synthetic ash used in all cases

Little effect of gas at 600°C

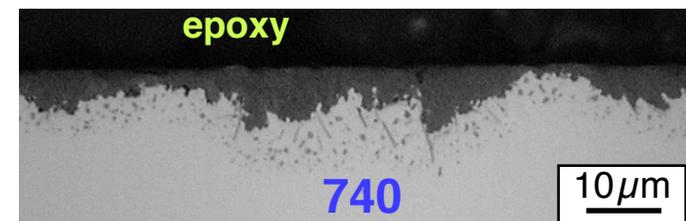
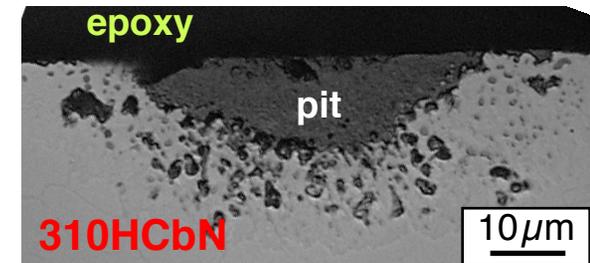
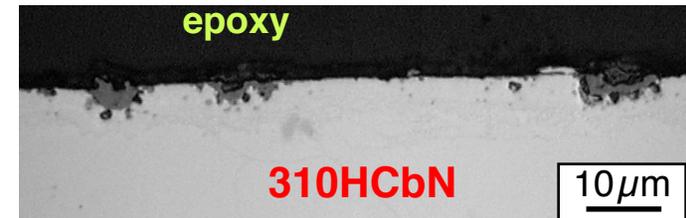
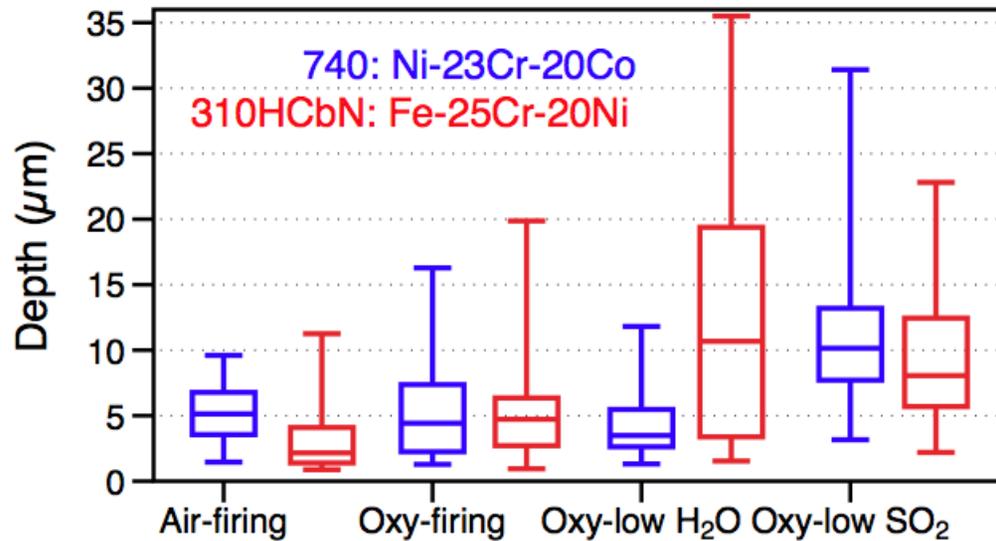
Synthetic coal ash, 500h exposures in 4 gases



Higher CO₂ environments not detrimental
Expected the lower SO₂ environment to lower attack
- same synthetic ash used in all cases

310-740 differences accurate?

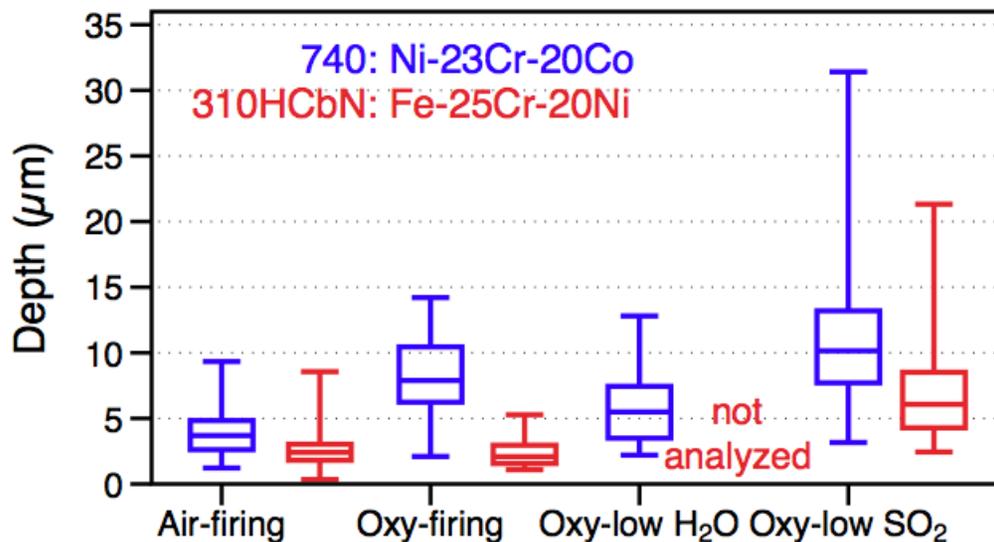
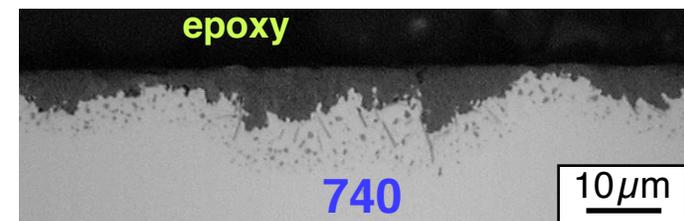
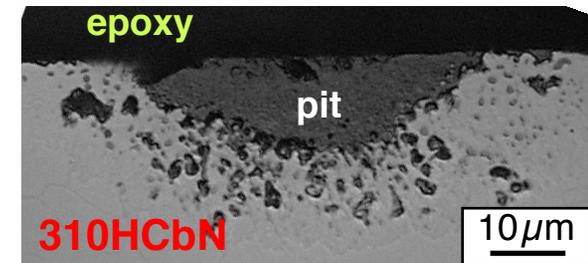
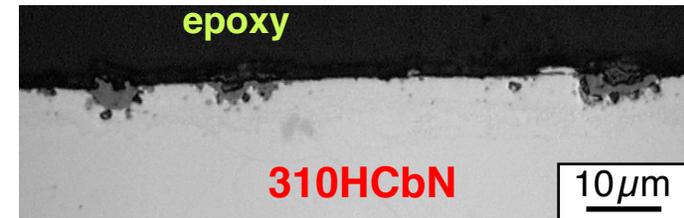
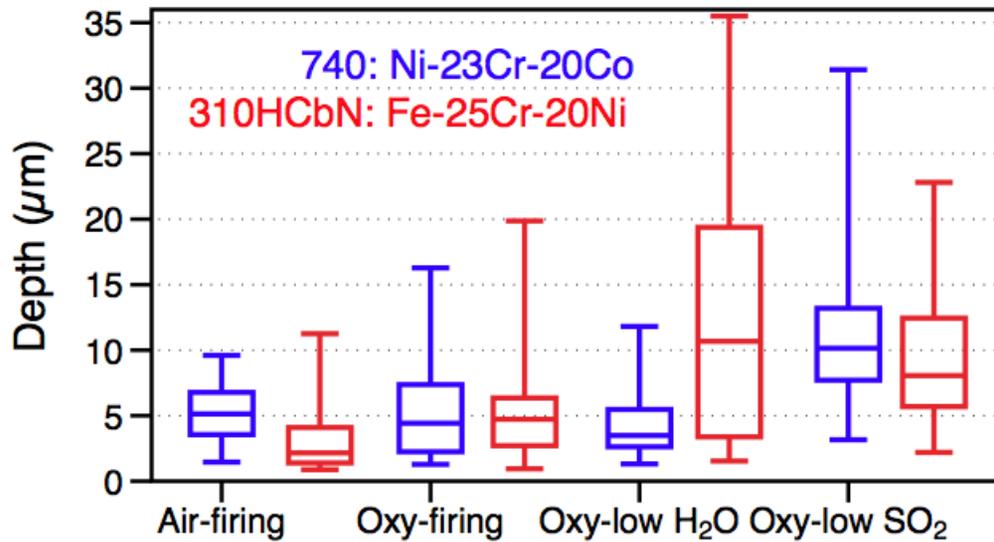
Highest alloyed examples with minimal attack



Sometimes focus on deepest penetrations
Need more images at “medium” magnification
Metal loss from 6mm diameter rod is minimal

Reanalyzed: 310HCbN < 740

High Ni-content alloy not most protective at 600°C



More accurate distributions from new images

Ash experiment issues

Experiments:

- air/oxy: worst case comparison
- “milder” oxy-firing: lower H₂O or SO₂
- add cold recirculation: low H₂O/low SO₂

Test protocols to be evaluated:

- use of Pt catalyst
- crucible (covered sample) vs. ash slurry
- cycle frequency 10 x 100h vs. 500h x ?
- goal: “actual” rate or accelerated?

Metal loss measurement

- box plots capture variable attack
- scale thickness (not rod diameter)

Ash composition: how changed by oxy-firing?

Summary: Creep in steam

1. 800°C:

completing work on Ni-base

740 (Ni-23Cr-20Co); 230 (Ni-22Cr-14W)

air vs. steam

in-situ vs. ex-situ

anneal (thermal effect)

2. 650°C:

Grade 91 (9Cr-1Mo)

air vs. steam

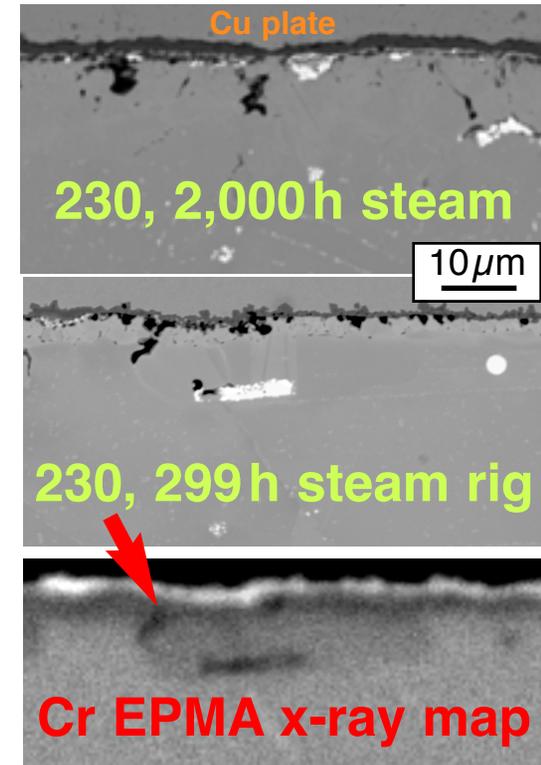
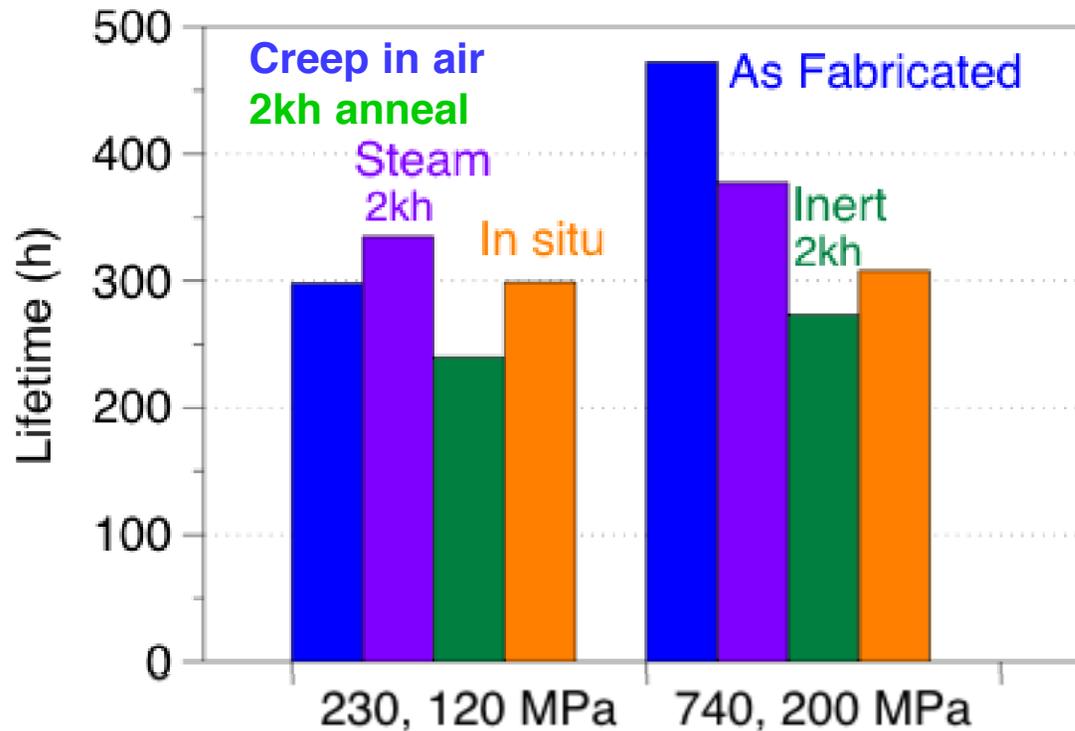
coated vs. uncoated

two in-situ creep rigs



800°C: 230/740 limited steam effect

Creep rupture tests in air and 1 bar steam



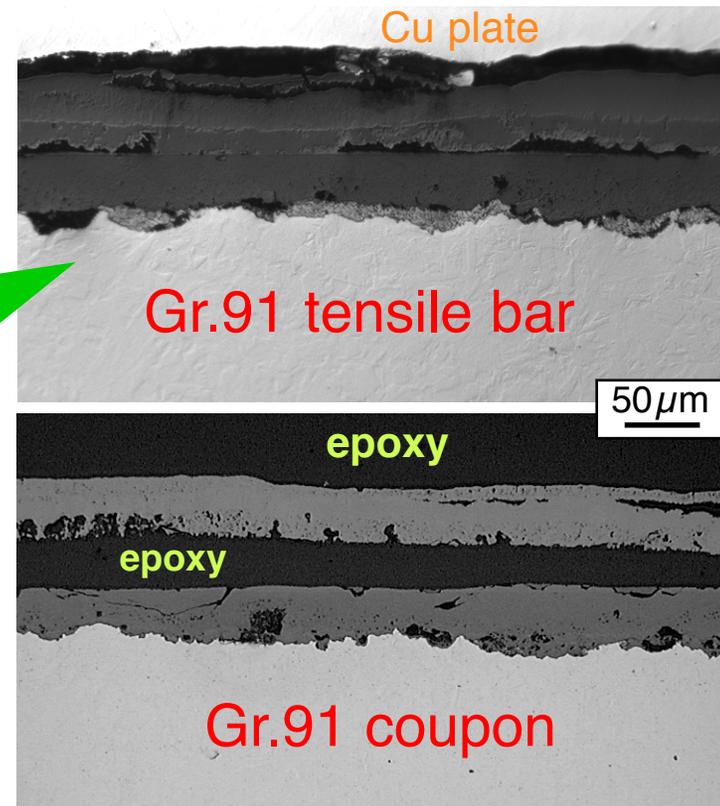
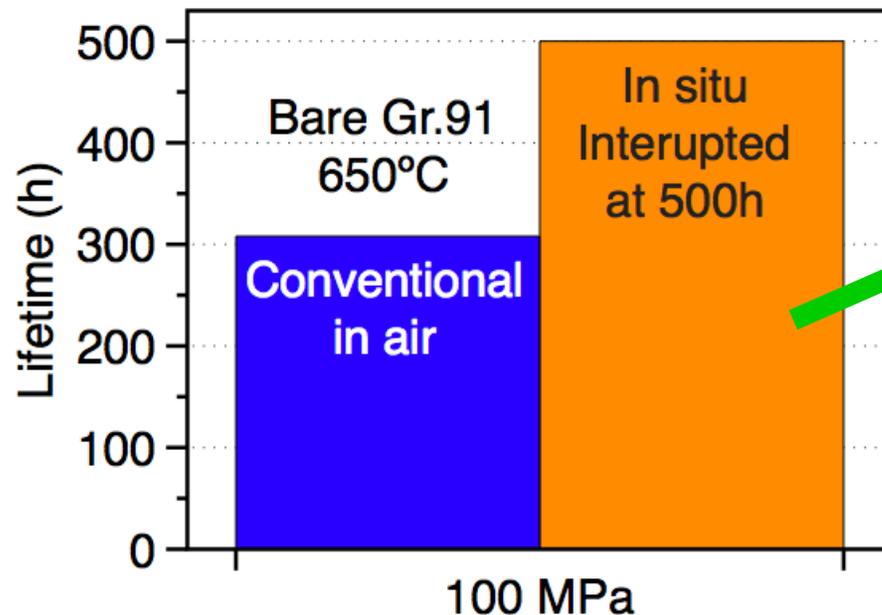
230: no effect of in-situ or ex-situ steam

740: microstructural reason for decreased life?

- alloy/oxide characterization in progress
- task will conclude this summer with paper

Grade 91: higher lifetime in steam

650°C 100MPa in air and 1 bar steam



650°C, 500h, 1 bar steam

Grade 91: Fe-9Cr-1Mo

Two concerns: temperature
load transfer

Verified similar oxide formed on coupon in steam

Milestones

FY11

- Done** - Procure coatings for creep testing (12/10)
- Done** - Initial assessment of CO₂ role (6/11)
- Done** - Complete 600°C coal ash testing (6/11)
- Delayed (9/11)**- In-situ 650°C creep testing
(Resource delays/followup on results)

FY12

- Done** - Report CO₂-H₂O effects (12/11)
- Done** - Complete 600°-650°C steam tests (3/12)
- Complete in-situ Ni-base creep testing (6/12)
- Complete 700°C coal ash characterization(9/12)

Summary

Four tasks: gas only, with ash, creep, coatings

Gas only: further work on 600°C CO₂ effect
650°C steam testing complete

Coal ash corrosion:

further data analysis of 600°C results

- Oxy-firing no worse with same ash

FY12 focus on temperature series

add “cold” oxy-firing conditions

Creep: T91 work at 650°C in progress

Ni-base: completing characterization

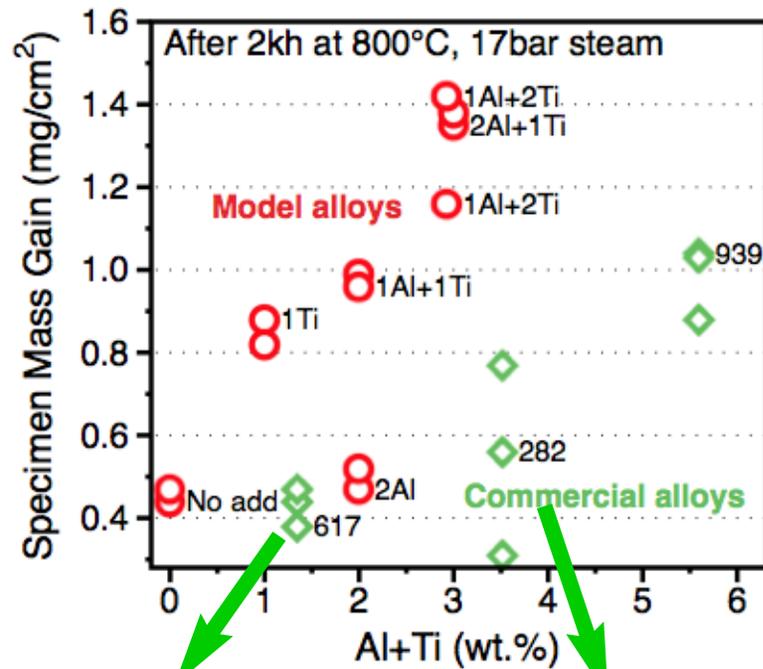
Coatings - final work on model/creep effects

CLEAN COAL. COOL.



800°C model Ni-22Cr alloys

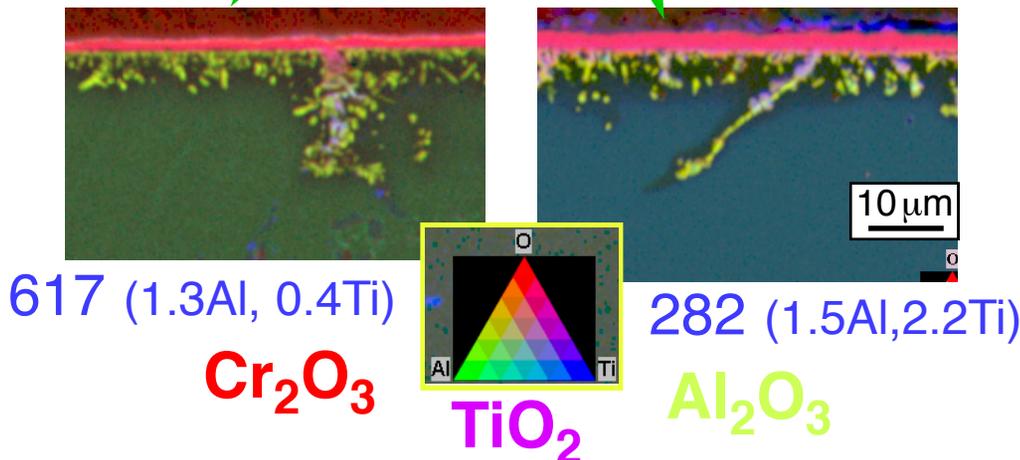
17bar steam, 2,000h exposure



Model alloys:
simulate Al,Ti effect
on internal oxidation

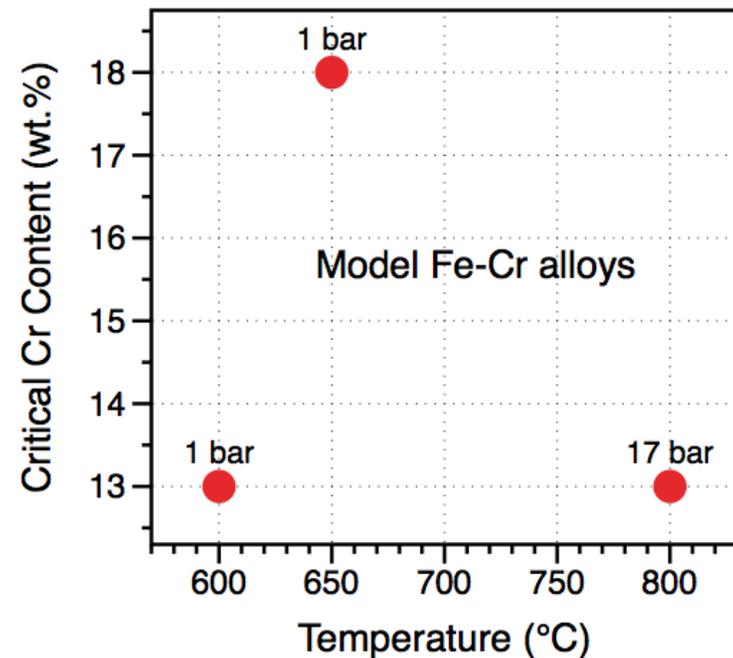
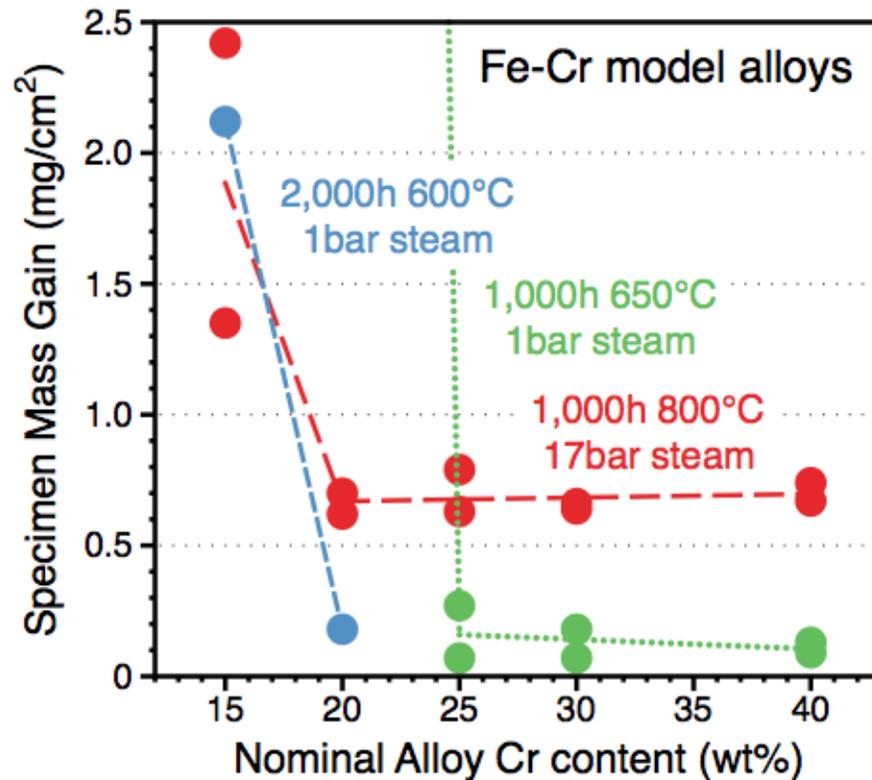
Ni-18Cr alloys (282)
fabricated (2)

Future:
quantify depth of attack
continue to 5,000h
expose to coal ash



Fe-xCr model binary alloys

1 and 17bar steam, 1-2 kh exposures



Here, model alloys perform worse than expected

Need to fill in with additional temperatures

Next question is about ternary additions (Mn, Si...)

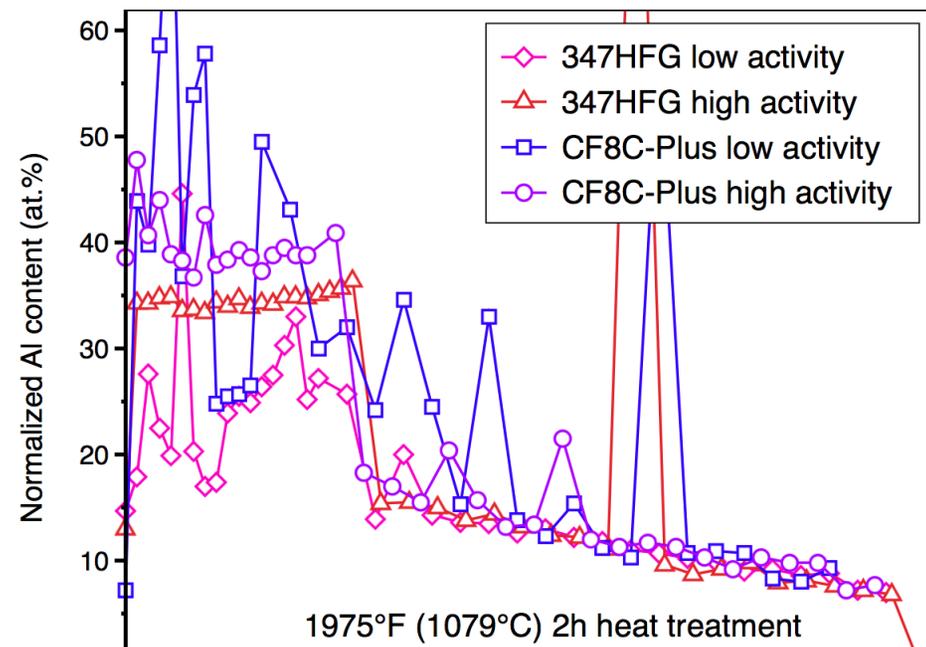
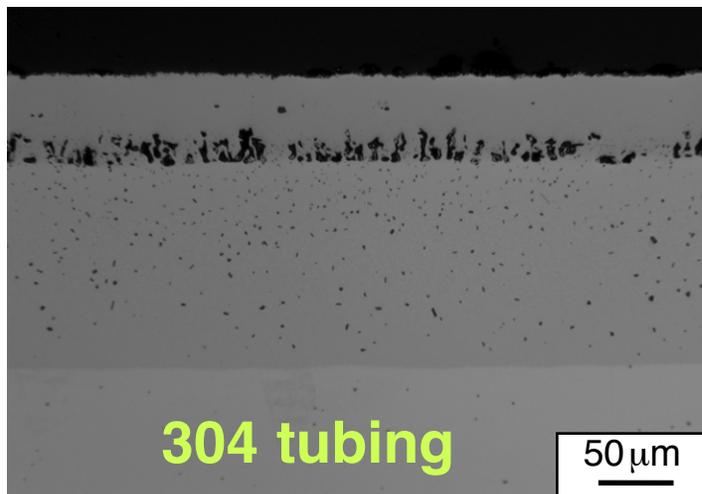
Coating commercialization (slow)

- No industry interest in coating 8-11%Cr steels
peak application is $\sim 600^{\circ}\text{C}$ - no interdiffusion
- More interest for austenitics (304, 347, etc.)
boiler application limited to $\sim 650^{\circ}\text{C}$
phase boundary will limit interdiffusion

304H/347H tube explosions created interest

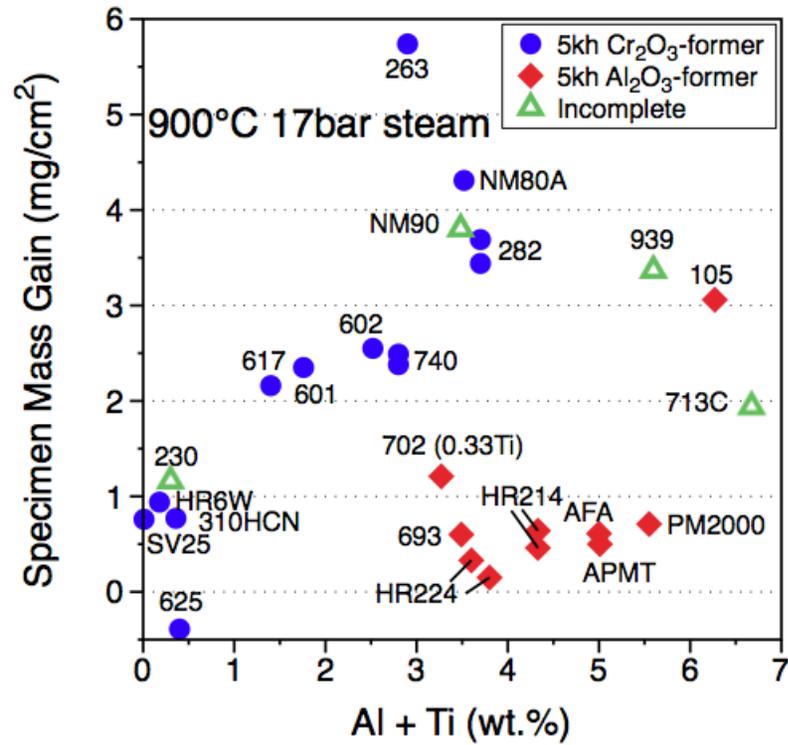
EPRI funding for coating demonstration:

Vapor slurry coating



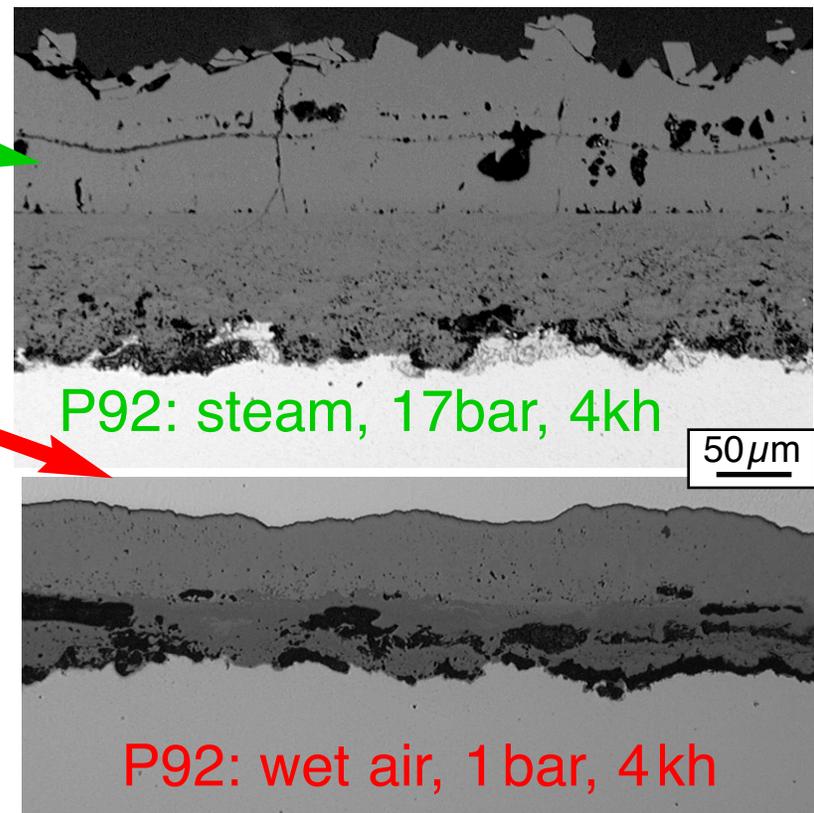
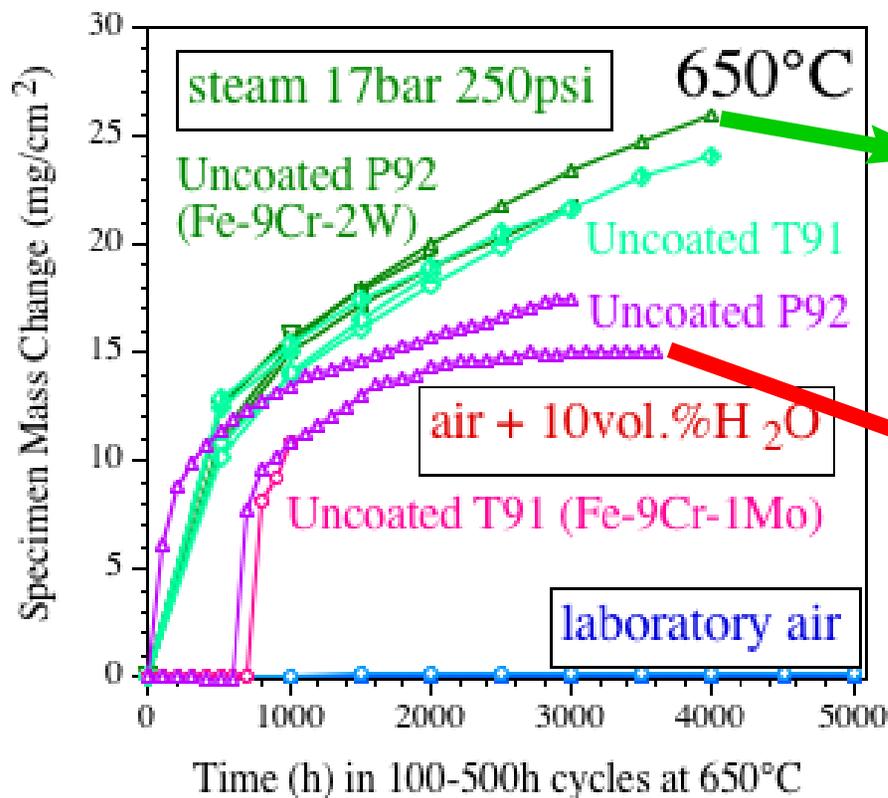
900°C steam

5,000h



Fe-9Cr in Steam vs. Humid Air

comparison of mass gain and reaction products
650°C, 1202°F



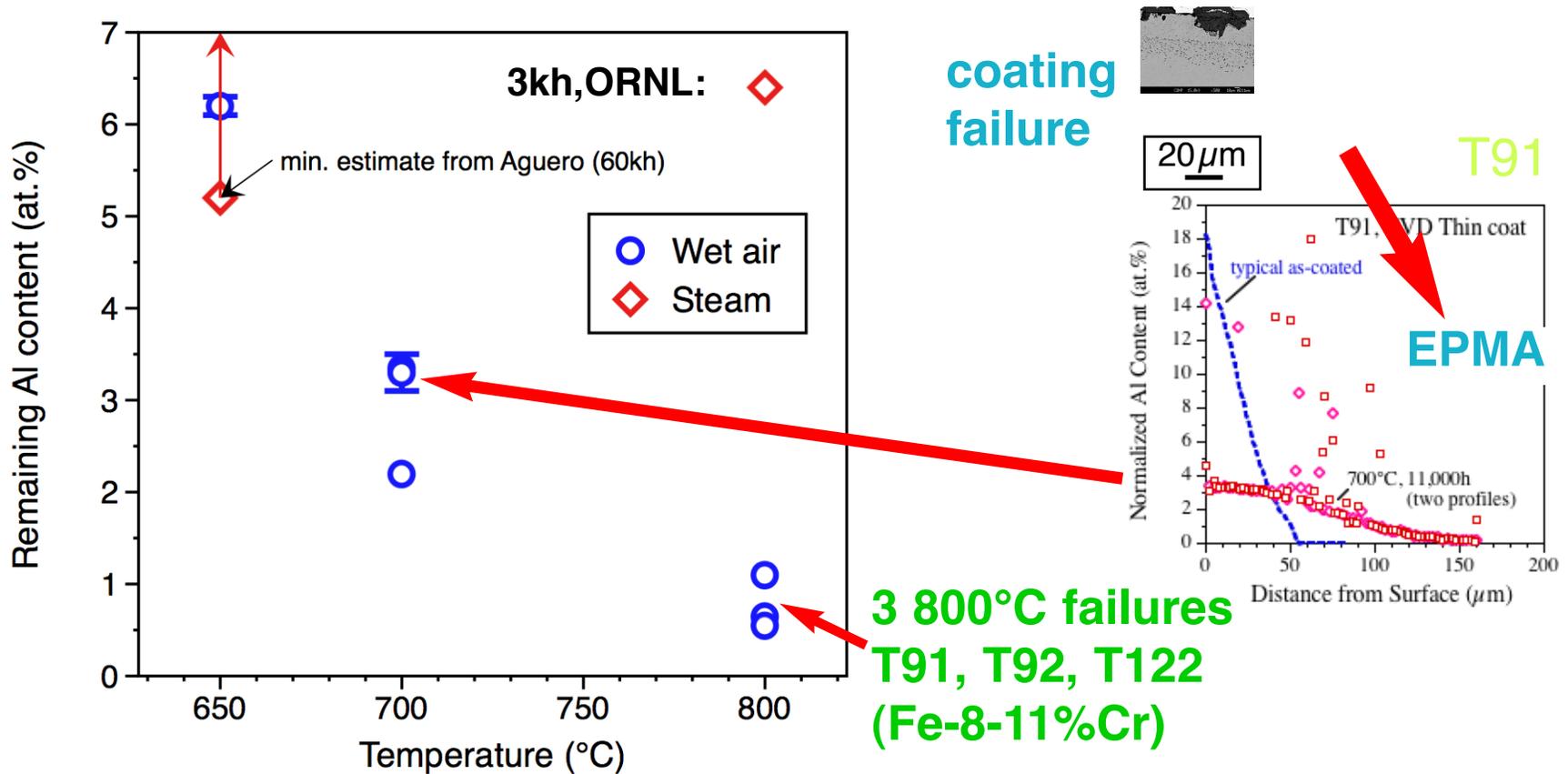
Similar attack in steam and wet air (10±1 vol.% H₂O)

Define failure: must have environment that attacks substrate

Prior work in lab. air could not define coating lifetime

Effect of temperature on C_b

$\sim 40\mu\text{m}$ coatings on Fe-Cr at $650^\circ\text{-}800^\circ\text{C}$ in H_2O

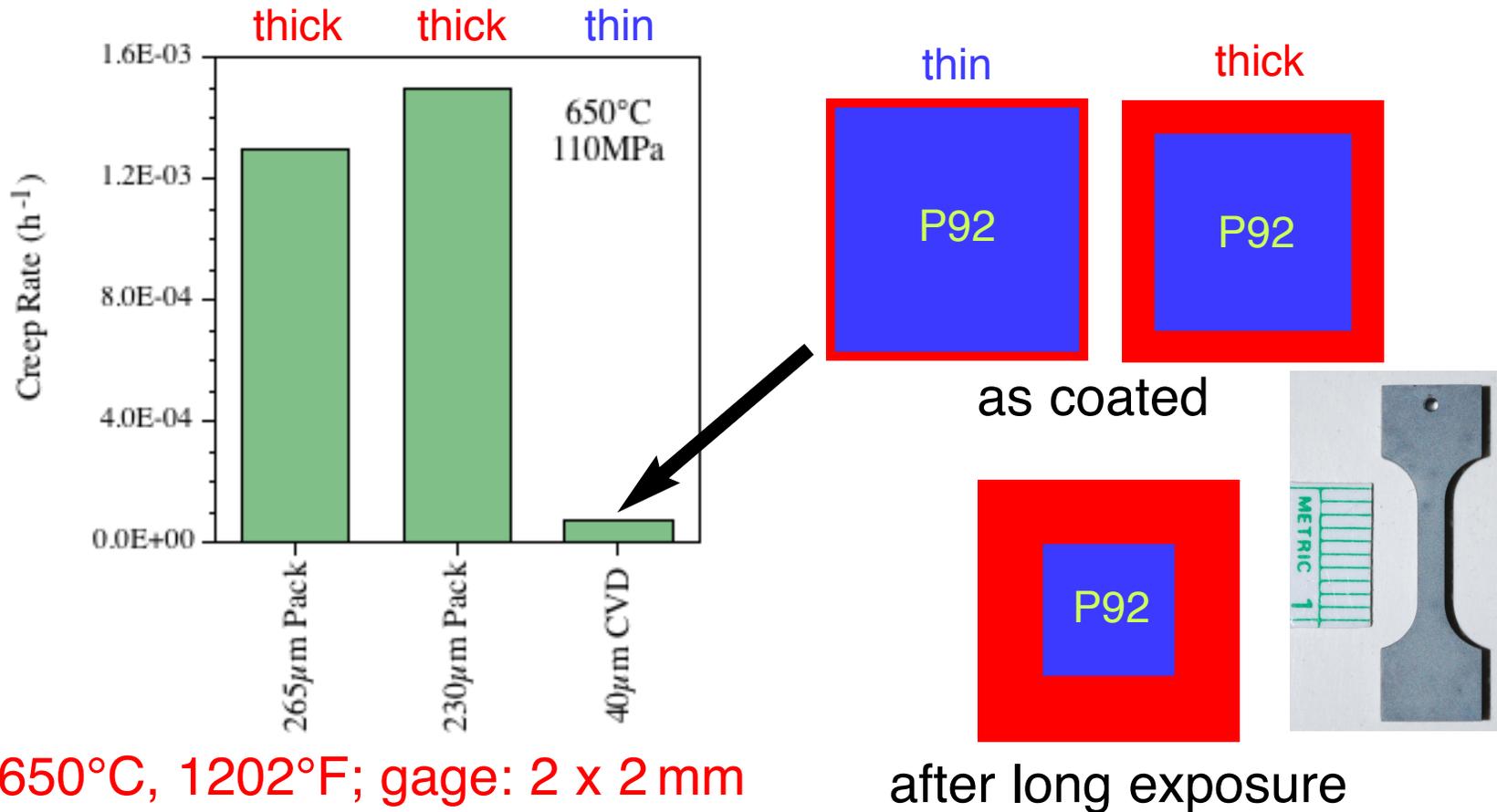


Six failures of thin coatings, one higher Al activity coating
Agüero: 650°C slurry coating failed at $\sim 60\text{kh}$ in steam

If temperature relationship is understood, this data set
forms the basis for a comprehensive lifetime model

Creep Testing of P92 (Fe-9Cr-2W)

Effect of as-deposited coating thickness



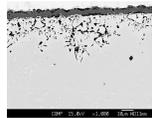
Specimen with thin coating has better creep resistance
Effect of coating can be modeled as if coated layer absent

Suggests that thin coatings are preferable

Dryepondt et al., Surf. Coat. Tech. (2006)

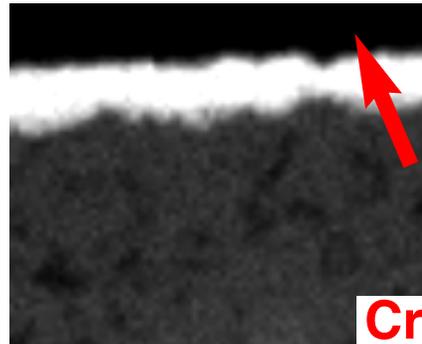
Unusual Ti distribution in scale

Cast alloy 282 after 5kh in steam at 800°C



cast 282

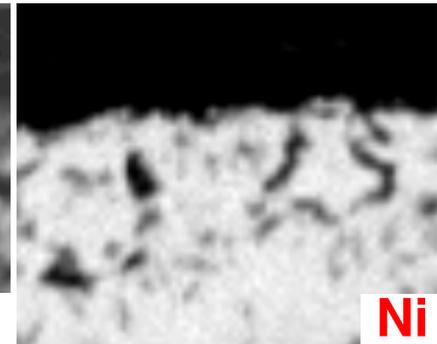
10 μm



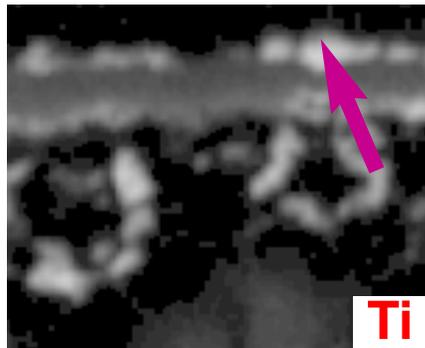
Cr



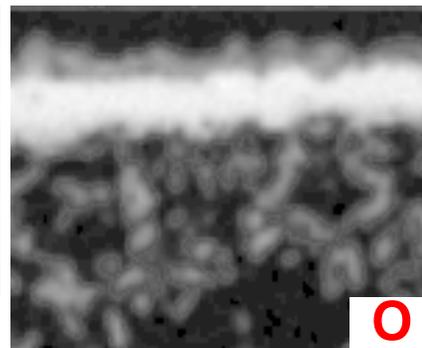
Al



Ni



Ti



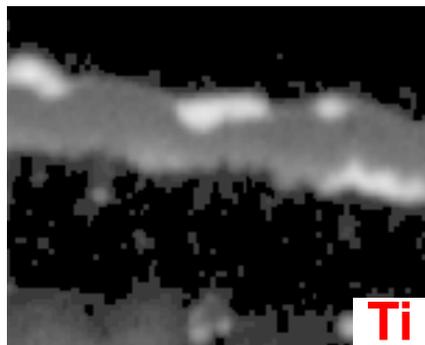
O

Electron probe analysis:

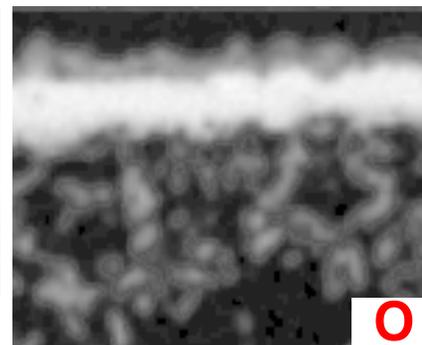
Typical internal Al + Ti oxidation

Ti “layer” at both gas & metal side

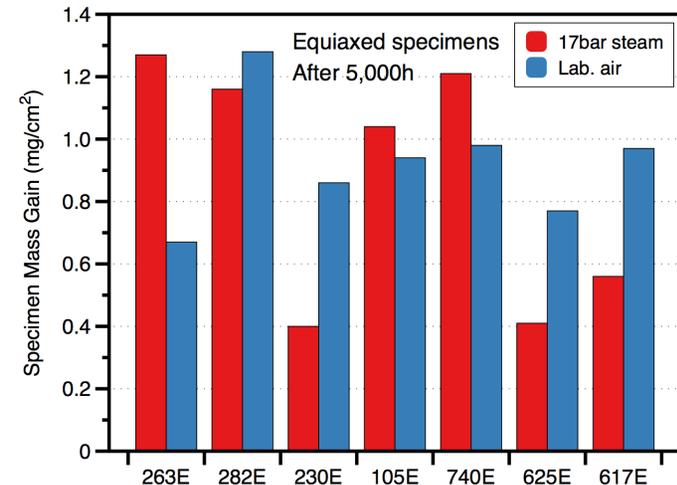
Scale after 5kh lab air:



Ti

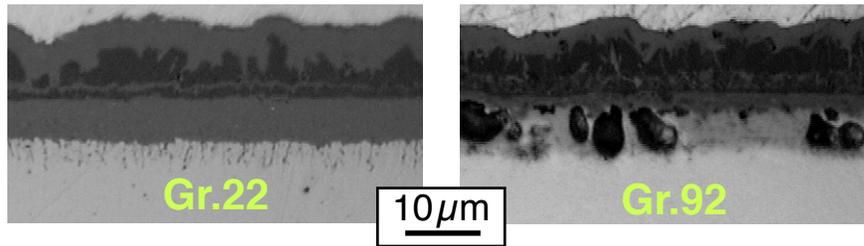


O

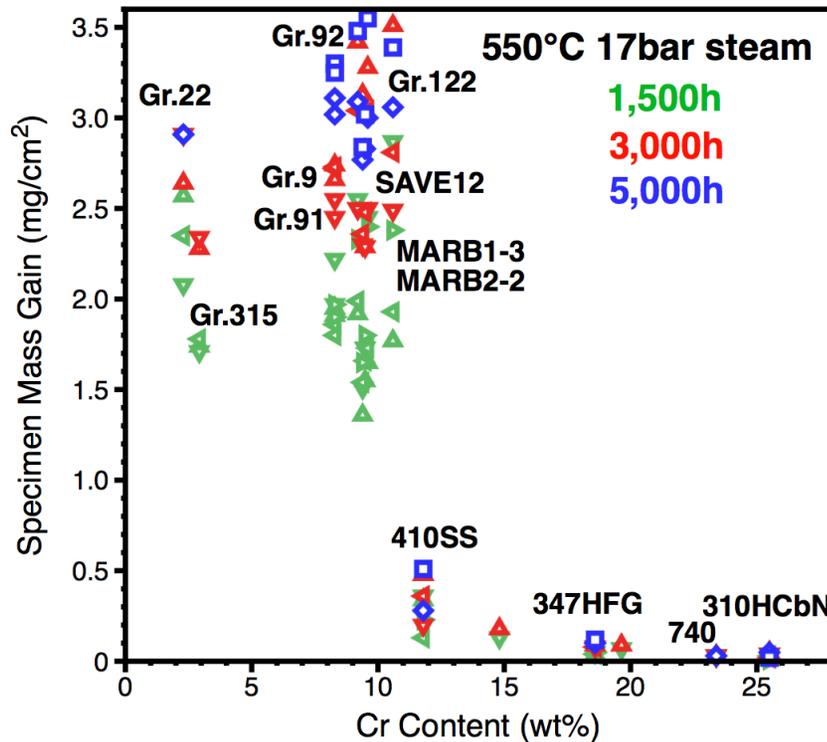


~12%Cr needed at 550°C

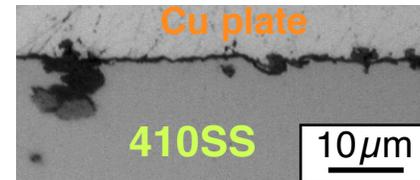
For protective behavior at 17bar steam



dual oxide layer



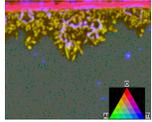
2,000 h 550°C



Surprisingly, little difference in 2.25-11%Cr steels
5,000h cross-sections in progress

800°C steam follow up work

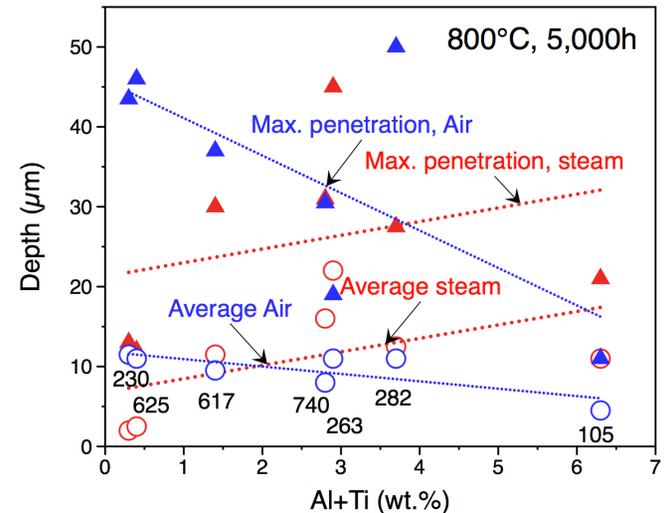
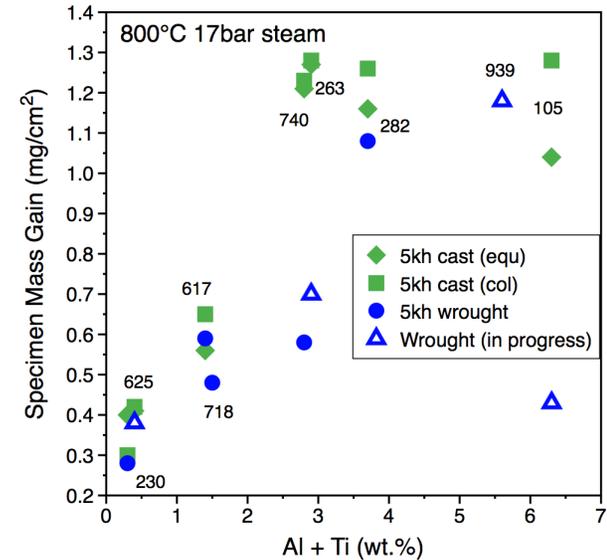
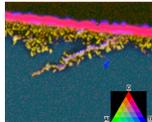
Alloy 282: 5kh in 17bar steam or lab. air



Ni~20Cr
Al+Ti-> γ'

Synergy
Al-Ti ?

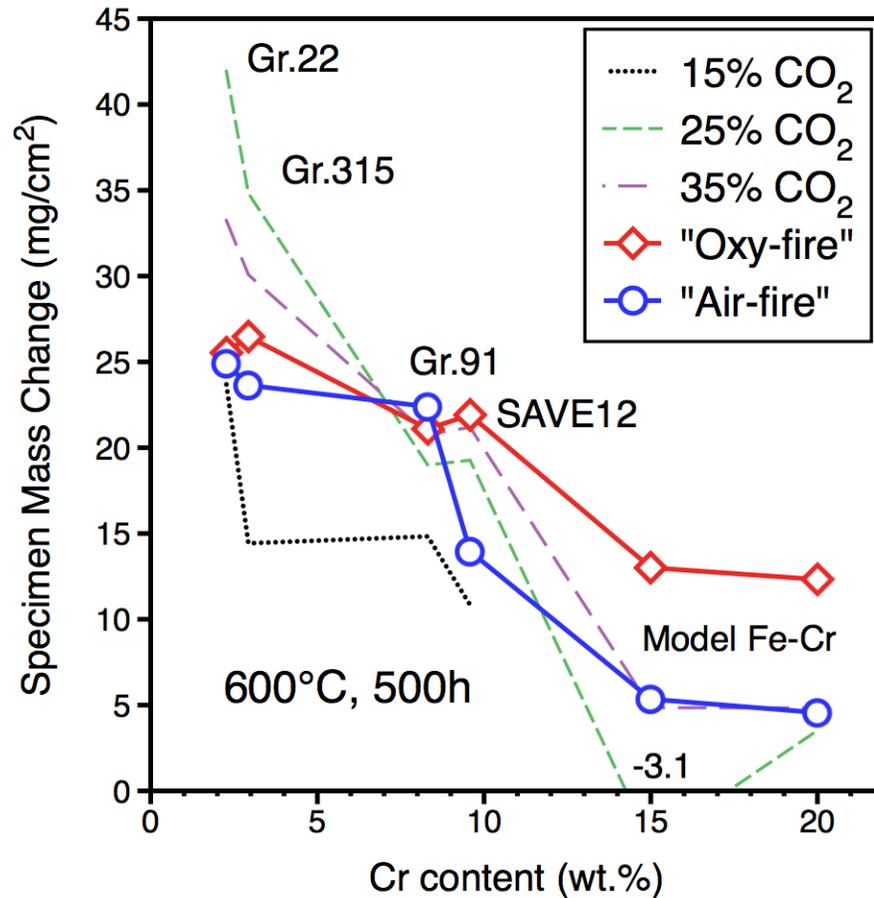
5 μm



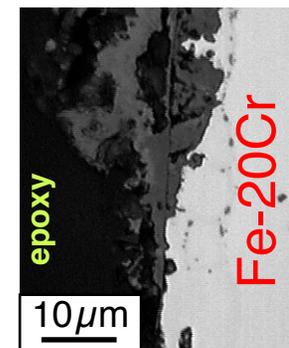
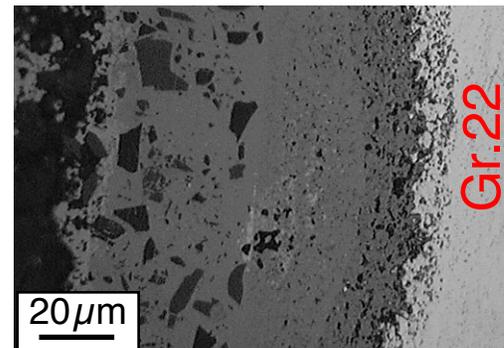
Model alloys: Ni-22Cr + Al +/- Ti in steam

New coal ash tests: H₂O added

Air- and Oxy-firing conditions: 600°C, 500h



| | | |
|------------------|------|----------------|
| | air | O ₂ |
| CO ₂ | 16 | 61% |
| H ₂ O | 10 | 32% |
| O ₂ | 2 | 2% |
| SO ₂ | 0.15 | 0.45% |



Modified gas train to add H₂O to test

Mass gain: not a strong effect of H₂O

Change to oxy-firing had strongest effect on high Cr

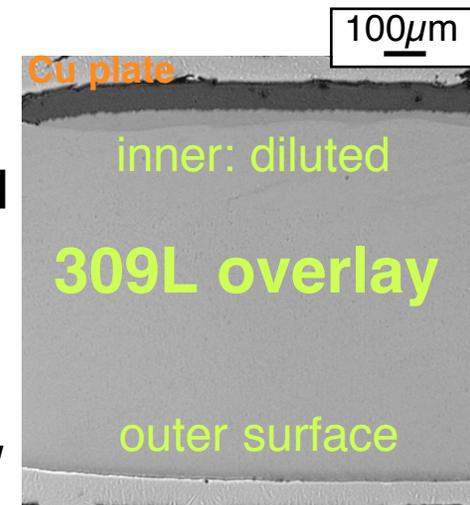
Evaluated weld-overlay coupons

Air- and Oxy-firing conditions: 600°C, 500h

Nominal composition wt.%

from Titanova

| | Fe | Ni | Cr | other |
|------|----|----|----|----------|
| 309L | 60 | 14 | 23 | 1Mn, 1Si |
| 8020 | | 80 | 20 | |
| 33 | 33 | 31 | 33 | 2Mo, 1Cu |
| 52 | 9 | 63 | 29 | |
| 72 | | 57 | 43 | 0.3Ti |
| C22 | 3 | 58 | 23 | 13Mo, 3W |



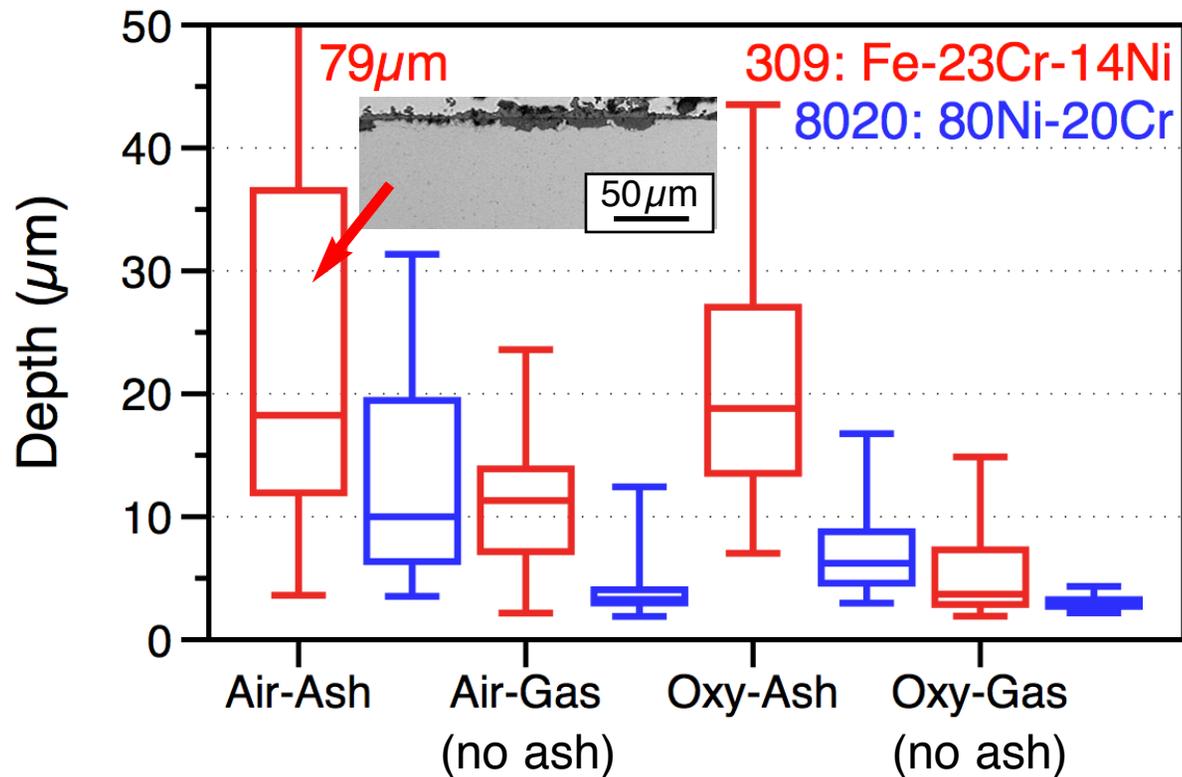
Rectangular coupons: removed overlay from tube

~1mm thick

- face adjacent to substrate has some dilution
- mass change data meaningless

Box plots to quantify attack

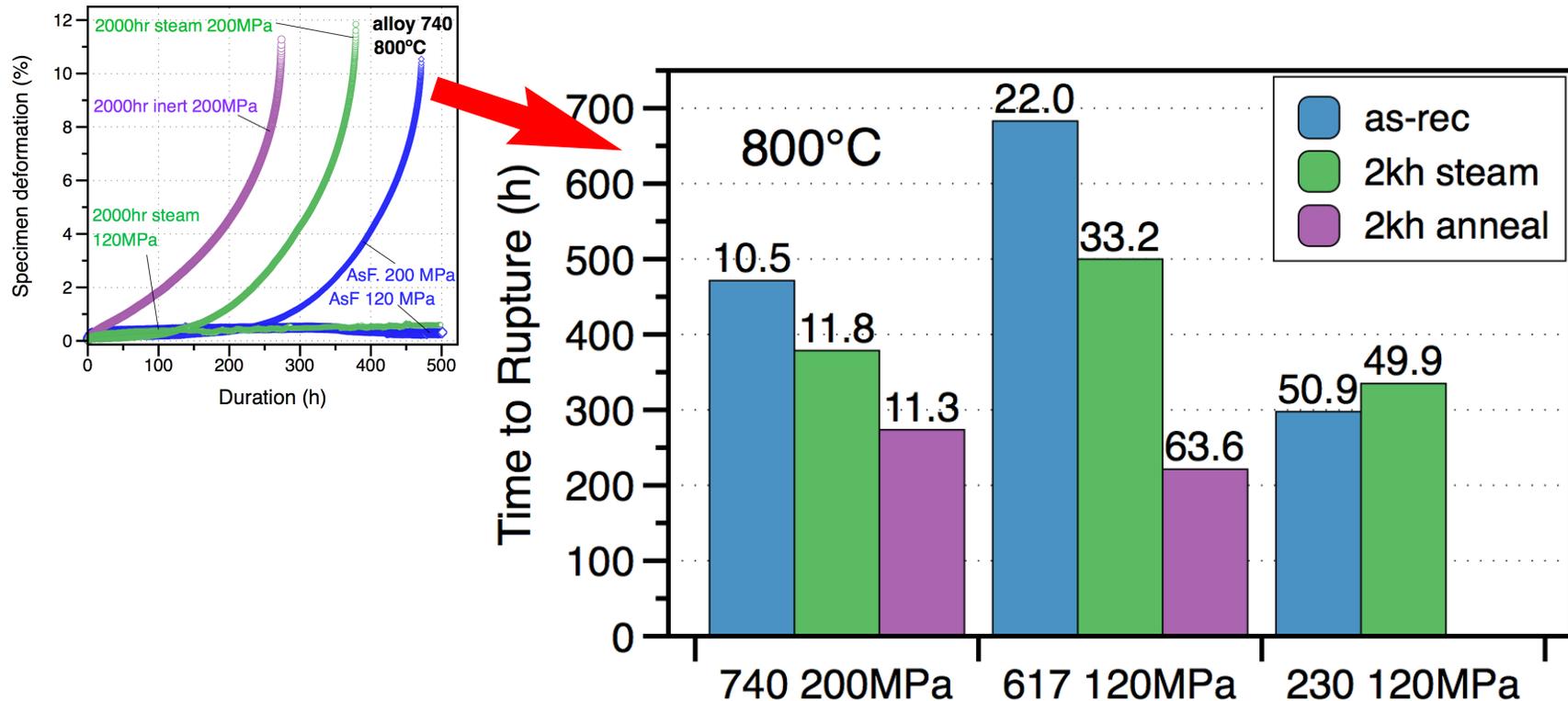
Air- and Oxy-firing conditions: 600°C, 500h



40 data points taken from 500X pictures
including scale + internal oxidation
high Ni coating more oxidation resistant
attack not increased in oxy-firing conditions

Ex-situ testing: anneal vs. steam

2kh anneal to account for thermal effect



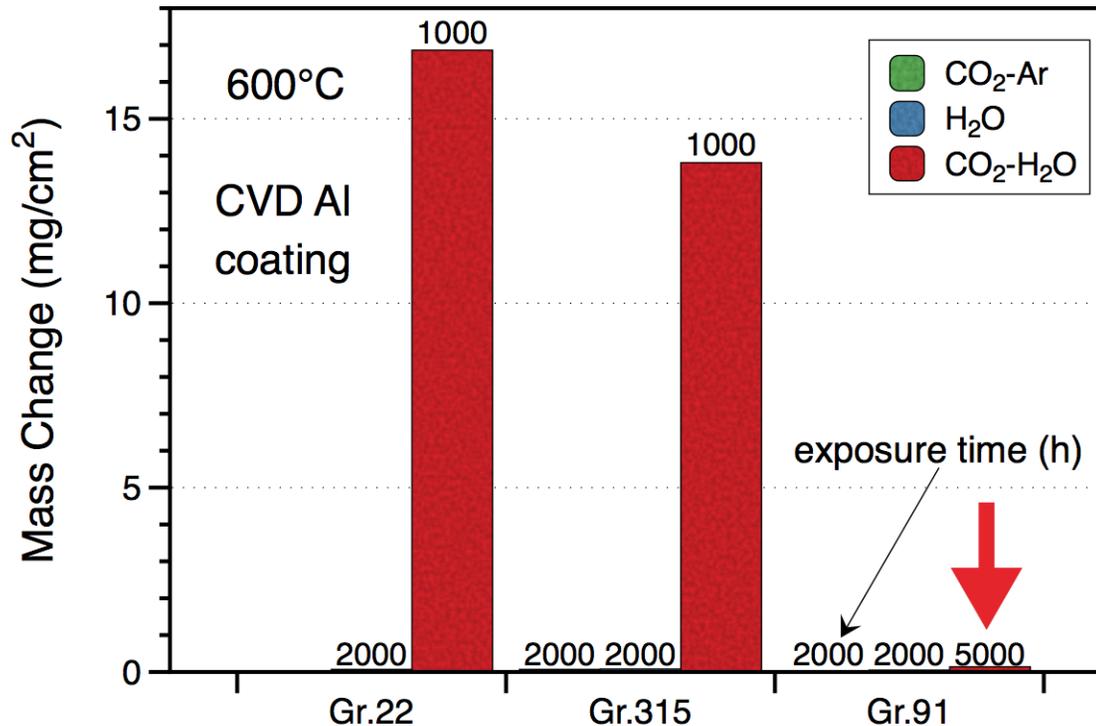
230: no effect of 2kh in steam at 800°C

740/617: decrease life after 2kh steam

larger decrease with 800°C 2kh anneal (?)

Coating results at 600°C

Low Al content chemical vapor deposition coating



Conclusions:

Coating prevents thick oxide formation in steam
Coating less effective on low Cr substrates
CO₂-H₂O is most aggressive environment